# Remediation of soil and groundwater Rizlan Bernier-Latmani Problem set # 4: vapor phase processes

## **Problem 1:**

A biofilter is used to remove toluene from the gas phase. The gas flow rate is Q= 0.3 m<sup>3</sup>/h, the influent concentration  $C_i$ = 560  $\mu$ g/L. Monod kinetics: k=120.3 mg toluene/g cell/min and  $K_S$ =17.4 mg/L air. The operational biomass concentration is X= 1g cells/L air flow.

What is the effluent concentration of toluene assuming a height of 1m?

### Problem 2:

Please calculate the height of an air-stripping tower to remove ethylbenzene from groundwater given the following information.

Influent concentration of ethylbenzene: 1 mg/L Target effluent concentration: 35  $\mu$ g/L Liquid flow rate  $Q_W$ = 643.45 L/min Column diameter= 0.915m Packing= 2.5 cm polyethylene Raschig rings  $D_L$ =6\*10<sup>-6</sup> cm<sup>2</sup>/s  $D_G$ =0.09404 cm<sup>2</sup>/s Air to water ratio: 100:1  $K_H$ '= 0.27 T= 20 °C.

### **Problem 3**:

A leaking underground storage tank has discharged 10 m<sup>3</sup> of 1,1,1-TCA to a sandy clay soil. The contaminated soil is found to extend over a diameter of approximately 30m and a depth of 10m, beginning 2m below the surface. A short SVE program at 3 m<sup>3</sup>/min or 4.5 m<sup>3</sup>/min was run to select the design extraction rate and the data are shown below. The extraction rate selected was Q=3 m<sup>3</sup>/min.

Estimate the time necessary to remove 95% of TCA.

Characteristics of 1,1,1-TCA: vapor pressure  $P_v$ = 0.13 atm at 20°C MW= 133.4 g/mol  $\rho_{TCA}$ =1,325 kg/m<sup>3</sup>  $K_H$ '=0.56 at 20°C  $K_{OW}$ =10<sup>-2.5</sup>

Soil characteristics:

Wet bulk density:  $\rho_{wb} = 2{,}090~kg/m^3$   $K_D \! = 10^{\text{-}5}~m^3/g$  (for 1,1,1-TCA)

 $\theta$ = 0.10 m<sup>3</sup>/m<sup>3</sup>  $\epsilon$ =0.25  $T_{soil}$ =20°C  $\rho_{air}$ =1.28 kg/m<sup>3</sup>

#### Problem 4:

A soil is contaminated with petroleum hydrocarbons and injection bioventing (with no gas phase treatment) or soil vapor extraction are being considered as treatment approaches. Due to the cost, only a single well at the center of the contamination area is planned and the injection and the extraction flow rates are set:

For injection: 60 m<sup>3</sup>/day For extraction: 120 m<sup>3</sup>/day

The question for the environmental engineer in charge of the site to solve is which treatment would be most rapid in this situation?

The contamination area is cylindrical and 6 meters deep and covers a surface area of  $20 \text{ m}^2$ .

The concentration of total petroleum hydrocarbon (TPH) is 500 mg TPH/kg soil and assumed to be homogeneously distributed. The target concentration is 50 mg TPH/kg soil. The dry bulk density of the sediment is 1,400 kg/m³.  $K_D$ =0.03 m³/kg and  $K_H$ =2.08[-], soil porosity  $\epsilon$ =0.3, soil moisture content  $\theta$  = 0.05; 1 g  $O_2$  is required to degrade 0.3 g of TPH carbon. As a reminder, the molar volume of gas is 22.4 L per mole under these conditions. The well is screened along the entire 6m of the contaminated soil depth.

The percent volume of  $O_2$  in air is  $C_{02}$ =21%  $m^3$   $O_2/m^3$  air

## Part 1: Bioventing

- 1- What is the oxygen utilization rate (in % m<sup>3</sup> O<sub>2</sub>/(m<sup>3</sup> air.day)) that is reached with this air flow rate?
- 2- What is the corresponding biodegradation rate of TPH (in mg TPH/(kg soil.day))?
- 3- Assuming the biodegradation rate follows first order kinetics, how long will the remediation take to reach the target with this method?

### Part 2: SVE

- 4- What is the concentration of TPH in the gas phase initially  $(C_{TPH,g})$ ?
- 5- How long will it take to reach the regulatory goal? (hint: consider that the total mass of TPH changes as it is removed by SVE)

Finally, please indicate what you think is the best approach here and why.